GUJARAT TECHNOLOGICAL UNIVERSITY

BE - SEMESTER-V (NEW) EXAMINATION – WINTER 2022

Subject Code:2151909 **Subject Name: Heat Transfer** Time:10:30 AM TO 01:00 PM

Date:04-01-2023

Total Marks:70

Instructions:

- 1. Attempt all questions.
- 2. Make suitable assumptions wherever necessary.
- 3. Figures to the right indicate full marks.
- 4. Simple and non-programmable scientific calculators are allowed.

| | | | Marks |
|-----|-------------|---|----------|
| Q.1 | (a) | Define: Fin performance and fin efficiency | 03 |
| | (b) (c) | Explain Stefan Boltzmann constant. Discuss velocity boundary layer and thermal boundary layer over a flat | 04 |
| | | plate. Show the thickness of these layers for different Prandtl numbers. | 07 |
| Q.2 | (a) (b) | Define: 1) Intensity of Radiation 2) Irradiation 3) Radiosity Making use of Plank's law of distribution, establish the relation for the Wien's displacement law | 03 04 |
| | (c) | A furnace wall is made of 20 cm of magnesite brick and 20 cm of common brick. The magnesite brick is exposed to hot gases at 1355 °C and common brick outer surface is exposed to 45 °C room air. The convection and radiation heat transfer coefficient towards air side are 12.5 and 7.5 W/m2 respectively. Thermal conductivities of magnesite and common brick are 3.8 and 0.66 W-m K respectively. Calculate a) heat loss per m2 area of furnace wall and b) maximum temperature to which common brick is subjected. | 07 |
| | | OR | |
| | (c) | Saturated steam at 110 °C flows inside a copper pipe (thermal conductivity 450 W/m K) having an internal diameter of 10 cm and and external diameter of 12 cm, the surface resistance on steam side is 12000 W/m2 and that on the outside surface of pipe is 18 W /m2 K. Calculate the heat loss from the pipe if it is located in space at 25 °C. | 07 |
| 0.3 | (a) | State Kirchoff's Law. | 03 |
| Q.5 | (b) | What is the fouling factor? Explain their effect in Heat Exchanger design. | 04 |
| | (c) | Atmospheric air at 25 °C flows parallel to a flat plate at a velocity of 3m/s. Use the exact Blasius solution to estimate the boundary layer thickness and the local skin friction coefficient at x=1 m from leading edge of the plate. Take $v = 15.33 \times 10^{-6} \text{ m}^2/\text{s}$. | 07 |
| Q.3 | (a) | State Fourier number and Biot number. | 03 |
| | (b) | Explain fundamental dimensions. State thermal resistance, thermal diffusivity and convective heat transfer coefficient in fundamental dimensions | 04 |
| | (c) | A polished metal pipe 5 cm outside diameter and 370K temperature at the outer surface is exposed at ambient conditions at 295 K temperature. The emissivity of surface is 0.2 and convection coefficient of heat transfer is 11.35 W/ m2 deg. Calculate the heat transfer by radiation and | 07 |

| | | natural convection per meter length of pipe. Take thermal radiation constant $\sigma_b = 5.67x~10\text{-}8~W/~m^2~K$ | |
|-----|--------------|---|----|
| Q.4 | (a) | Define shape factor. What is shape factor with respect to itself if the surface is concave, convex or flat? | 03 |
| | (b) | Describe the following dimensionless numbers for: Grashoff number 2) Nusselt number | 04 |
| | (c) | Derive the interchange factor for infinite parallel planes between non- black bodies | 07 |
| | | OR | |
| Q.4 | (a) | Compare Sub cooled and Saturated boiling. | 03 |
| | (b) | Explain the phenomenon of heat transfer by natural and forced convection | 04 |
| | (c) | Calculate the rate of heat loss from a human body which may be considered as a vertical cylinder, 30 cm in diameter and 175 cm high in still air at 15 °C. The skin temperature is 35 °C and emissivity at the skin surface is 0.4. For air: $v = 15.33 \times 10^{-6} \text{ m}^2/\text{s}$, $k = 0.026 \text{ W/m}$ deg. Laminar flow: $10^4 < \text{GrPr} < 10^9$, $\text{Nu} = 0.53 (\text{GrPr})^{0.25}$ Turbulent flow: $10^9 < \text{GrPr} < 10^{12}$, $\text{Nu} = 0.13 (\text{GrPr})^{0.33}$ | 07 |
| 0.5 | (a) | Differentiate between Recuperator and Regenerator Heat exchanger | 03 |
| Q | (b) | What is critical radius of insulation? Explain its importance in electrical and thermal system. | 04 |
| | (c) | Establish an expression for log mean temperature difference for parallel flow heat exchanger | 07 |
| | | OR | |
| Q.5 | (a) | Define: 1) Effectiveness and NTU related to Heat Exchanger | 03 |
| - | (b) | Explain with neat sketch, the various regimes in boiling and explain the condition for the growth of bubbles. | 04 |
| | (c) | Hot water having specific heat 4200 J/kg K flows through a heat exchanger at the rate of 4 kg/min with an inlet temperature of 100°C. A cold fluid having a specific heat 2400 J/kg k flows in at a rate of 8 kg/min and with inlet temperature 20°C. Calculate the maximum possible effectiveness if the fluid flow conforms to a) parallel flow arrangement b)counter flow arrangement. | 07 |
