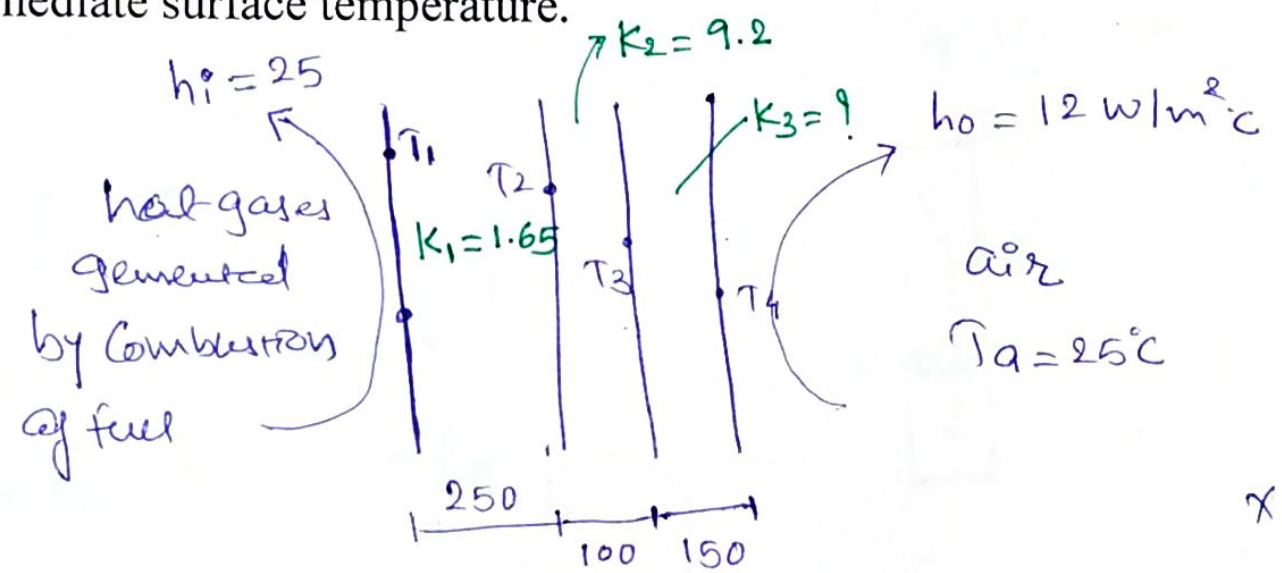
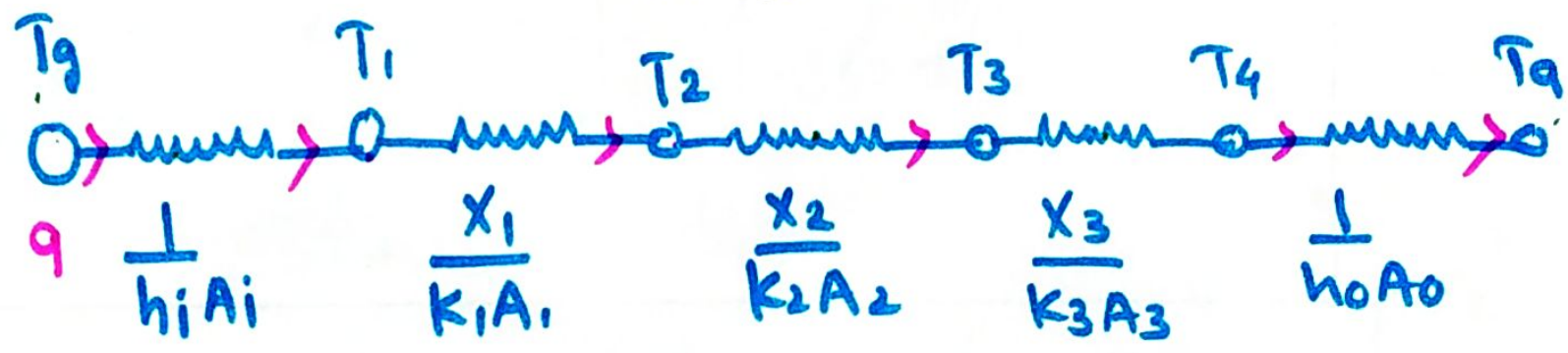


Q.1 A furnace wall is made up of three layers of thickness 250 mm, 100 mm and 150 mm with thermal conductivity of 1.65 and 9.2 W/m°C respectively. The inside is exposed to gases at 1250°C with a convection coefficient of 25 W/m²°C and the inside surface is at 1100°C, the outside surface is exposed to air at 25°C with convection coefficient of 12 W/m²°C. Determine The overall heat transfer coefficient, thermal conductivity of third layer, heat transfer rate per unit area and intermediate surface temperature.

- $U = ?$
- $K_3 = ?$
- $q/A = ?$
- $T_2 = ?$
- $T_3 = ?$
- $T_4 = ?$
- $T_g = 1250^\circ\text{C}$
- $T_1 = 1100^\circ\text{C}$
- $T_a = 25^\circ\text{C}$
- $K_1 = 1.65$
- $K_2 = 9.2$



- $h_i = 25$
- $h_o = 12 \text{ W/m}^2\text{C}$
- $T_g = 1250^\circ\text{C}$
- $T_a = 25^\circ\text{C}$
- $x_1 = 250 \text{ mm}$
- $x_1 = \cancel{250} \text{ mm}$
- $x_1 = 250 \times 10^{-3} \text{ m}$
- $x_2 = 100 \text{ mm}$
- $= 100 \times 10^{-3}$
- $x_3 = 150 \times 10^{-3} \text{ m}$



$$q = h_i A_i (T_g - T_i)$$

$$\frac{q}{A} = h_i (T_g - T_i)$$

$$= 25 (1250 - 1100)$$

$$= 3750 \text{ W/m}^2$$

$$q = \frac{(T_g - T_q)}{R_{\text{total}}}$$

$$R_{\text{total}} = R_1 + R_2 + R_3 + R_4 + R_5$$

$$R_{\text{total}} = \frac{1}{h_i A_i} + \frac{x_1}{k_1 A_1} + \frac{x_2}{k_2 A_2} + \frac{x_3}{k_3 A_3} + \frac{1}{h_o A_o}$$

$$R_{\text{total}} = \frac{1}{A} \left[\frac{1}{25} + \frac{250 \times 10^{-3}}{1.65} + \frac{100 \times 10^{-3}}{9.2} + \frac{150 \times 10^{-3}}{k_3} + \frac{1}{12} \right]$$

$$q = T_g - T_q$$

$$\frac{1}{A} \left[\frac{1}{25} + \frac{250 \times 10^{-3}}{1.65} + \frac{100 \times 10^{-3}}{9.2} + \frac{150 \times 10^{-3}}{k_3} + \frac{1}{12} \right]$$

$$\frac{q}{A} = \frac{1250 - 25}{0.04 + 0.1515 + 0.0163 + \frac{0.15}{k_3} + 0.0833}$$

$$3750 = \frac{1225}{0.2911 + \frac{0.15}{k_3}}$$

$$k_3 = 2.817 \text{ W/m}^\circ\text{C}$$

Overall heat transfer co-efficient-

$$U = \frac{1}{R_{\text{total}}}$$

$$R_{\text{total}} = \frac{1}{25} + \frac{0.25}{1.65} + \frac{0.15}{2.817} + \frac{0.1}{9.2} + \frac{1}{12}$$
$$= 0.3266 \text{ } ^\circ\text{C m}^2/\text{W}$$

$$U = \frac{1}{R_{\text{total}}}$$

$$= \frac{1}{0.3266} = 3.06 \text{ W/m}^2\cdot^\circ\text{C}$$

$$T_3 = 398.6^\circ\text{C}$$

$$T_4 = 337.5^\circ\text{C}$$

$$q = \frac{T_1 - T_2}{\frac{x_1}{k_1 A_1}}$$

$$3750 = \frac{1100 - T_2}{0.25/1.65}$$

$$T_2 = 531.8^\circ\text{C}$$

$$q = \frac{T_2 - T_3}{\frac{x_2}{k_2 A_2}}$$

$$q = \frac{T_3 - T_4}{\frac{x_3}{k_3 A_3}}$$

Q.2 The walls of a refrigerated truck consist of 1.2 mm thick steel sheet ($k=18 \text{ W/m-K}$) at the outer surface, 22 mm thick cork ($k=0.04 \text{ W/m-K}$) on the inner surface. Consider Heat transfer coefficient of $5 \text{ W/m}^2\text{-K}$ (between inside air and inside surface) and Heat transfer coefficient of $30 \text{ W/m}^2\text{-K}$ (between outside air and outside surface). The temperatures at the inside and outside air are 0°C & 35°C respectively. Calculate (1) heat transfer rate (2) steel-cork interface temp.

$$t_s = 1.2 \text{ mm} \\ = 1.2 \times 10^{-3} \text{ m}$$

$$t_c = 22 \text{ mm}$$

$$t_c = 22 \times 10^{-3} \text{ m}$$

$$k_s = 18 \text{ W/mK}$$

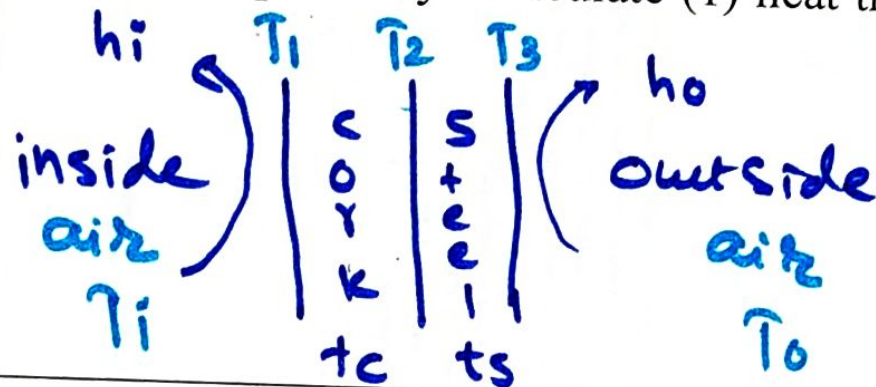
$$k_c = 0.04 \text{ W/mK}$$

$$h_i = 5 \text{ W/m}^2\text{K}$$

$$h_o = 30 \text{ W/m}^2\text{K}$$

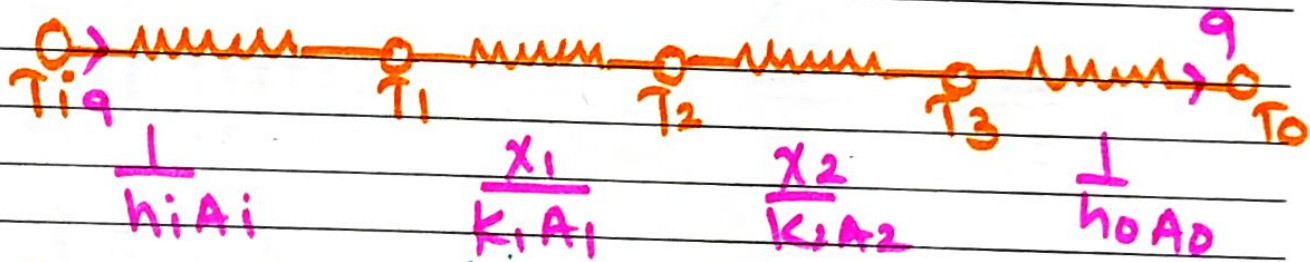
$$T_i = 0^\circ\text{C}$$

$$T_o = 35^\circ\text{C}$$



$$Q = ?$$

$$T_2 = ?$$



$$R_{\text{total}} = R_1 + R_2 + R_3 + R_4$$

$$Q = \frac{T_i - T_o}{R_{\text{total}}}$$

$$\frac{q}{A} = \frac{35}{\frac{1}{h_i} + \frac{T_c}{k_c} + \frac{\hat{T}_s}{k_s} + \frac{1}{h_o}}$$

$$\frac{q}{A} = \frac{35}{\frac{1}{5} + \frac{22 \times 10^{-3}}{0.04} + \frac{1.2 \times 10^{-3}}{18} + \frac{1}{30}}$$

$$= \frac{35}{0.2 + 0.55 + 6660 \times 10^{-5} + 0.033}$$

$$\frac{q}{A} = \frac{35}{0.7834}$$

$$\boxed{\frac{q}{A} = 44.67 \text{ W/m}^2}$$

$$\boxed{\hat{T}_2 = 15.63}$$

$$q = h_i A_i (T_i - \hat{T}_1)$$

$$\frac{q}{A} = h_i (T_i - \hat{T}_1)$$

$$44.67 = 5 \times (0 - \hat{T}_1)$$

$$\hat{T}_1 = 8.93$$

$$q = \frac{(\hat{T}_1 - T_2)}{\frac{T_c}{k_c \times A}}$$

$$\frac{q}{A} = \frac{(T_1 - T_2)}{T_c / k_c}$$

$$44.67 = \frac{8.93 - T_2}{0.022}$$

Q.3 A steam pipe pipe is covered with two layers of insulation, first layer being 3 cm thick and second 5 cm. the pipe is made from steel ($k = 58 \text{ W/m-K}$) having ID of 160 mm and OD of 170 mm. The inside and outside film coefficients are 30 and $5.8 \text{ W/m}^2\text{-K}$, resp. Draw electrical analogy for system and calculate the heat lost per meter of pipe, if the steam temperature is 300°C and air temperature is 50°C . The thermal conductivity of two materials are 0.17 and 0.093 W/m-K , resp.

$$q = \frac{T_s - T_a}{R_{\text{total}}}$$

$$q = \frac{(T_s - T_a)}{\frac{1}{h_i A_i} + \frac{1}{2\pi k_1 L} \ln\left(\frac{r_2}{r_1}\right) + \frac{1}{2\pi k_2 L} \ln\left(\frac{r_3}{r_2}\right) + \frac{1}{2\pi k_3 L} \ln\left(\frac{r_4}{r_3}\right) + \frac{1}{h_o A_o}}$$

$$q = \frac{(300 - 50)}{1.134} = 220.5 \text{ W/m}$$

$$r_1 = 80 \text{ mm}$$

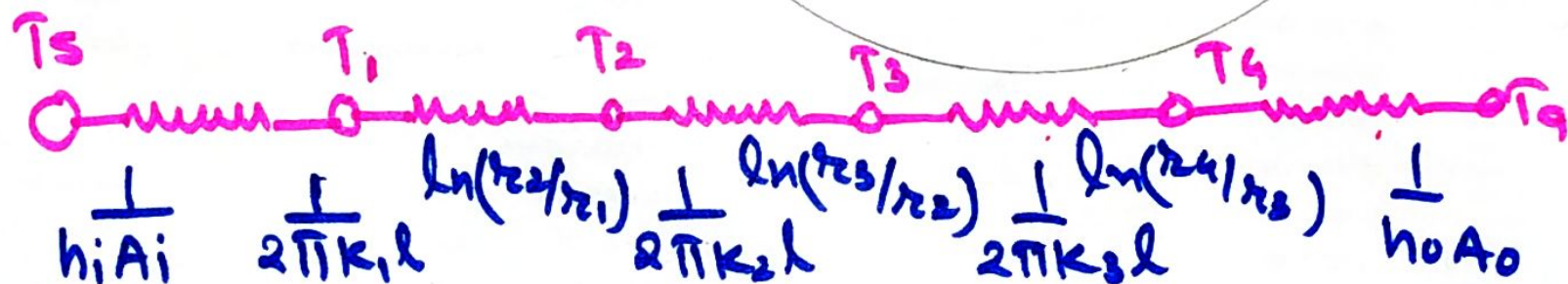
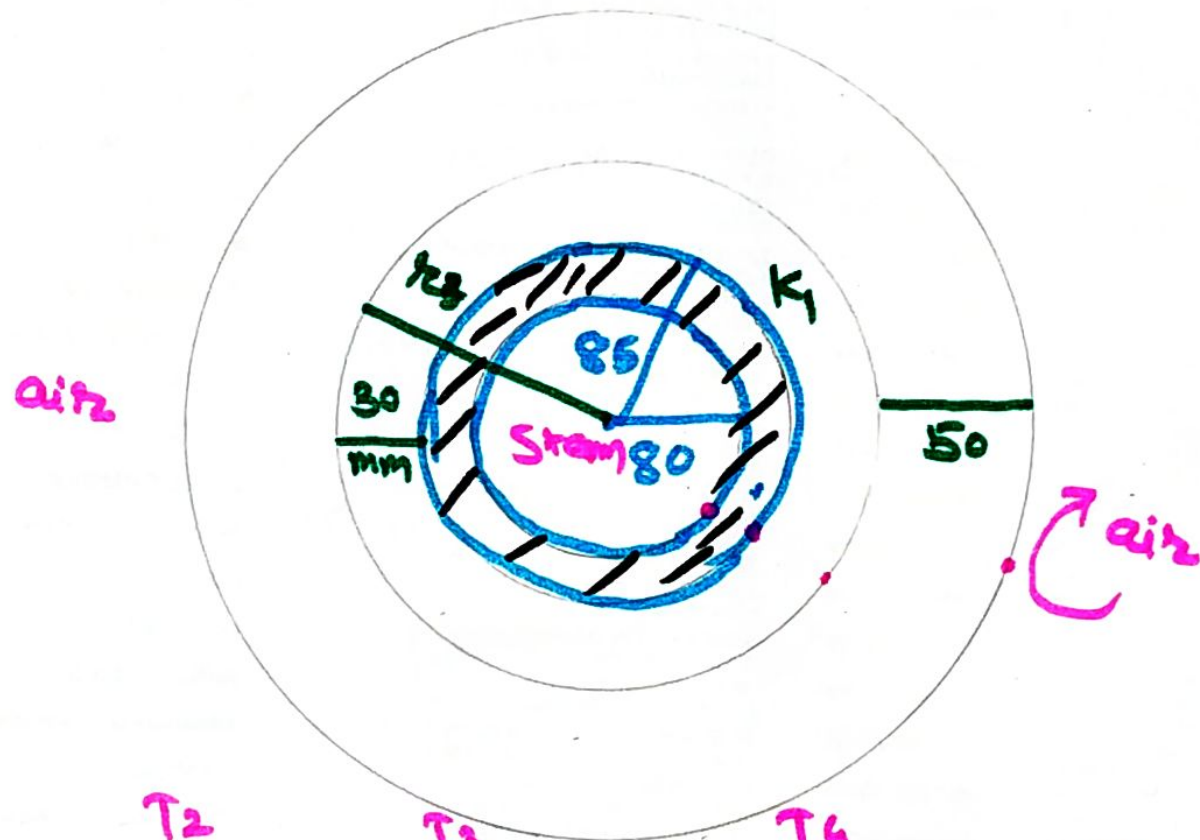
$$r_2 = 85 \text{ mm}$$

$$K_1 = 0.17$$

$$r_3 = 85 + 30 \\ = 115 \text{ mm}$$

$$r_4 = 115 + 50 \\ = 165 \text{ mm}$$

$$K_2 = 0.093$$



$$\begin{aligned}
 R_1 &= \frac{1}{h_i A_i} \\
 &= \frac{1}{30 \times 2\pi r_1 l} \\
 &= \frac{1}{30 \times 2\pi \times \frac{80}{1000} \times 1}
 \end{aligned}$$

$$R_1 = 0.0663 \text{ K/W}$$

$$\begin{aligned}
 R_2 &= \frac{\ln(r_2/r_1)}{2\pi k l} \\
 &= \frac{\ln(85/80)}{2\pi \times 58 \times 1}
 \end{aligned}$$

$$R_2 = 1.663 \times 10^{-4} \text{ K/W}$$

$$\begin{aligned}
 R_3 &= \frac{\ln(r_3/r_2)}{2\pi k_1 l} \\
 &= \frac{\ln(115/85)}{2\pi \times 0.17 \times 1} \\
 &= 0.283 \text{ K/W}
 \end{aligned}$$

$$\begin{aligned}
 R_4 &= \frac{\ln(r_4/r_3)}{2\pi k_2 l} \\
 &= \frac{\ln(165/115)}{2\pi \times 0.093 \times 1} \\
 &= 0.618
 \end{aligned}$$

$$R_{\text{total}} = 1.134$$

$$\begin{aligned}
 R_5 &= \frac{1}{h_o A_o} \\
 &= \frac{1}{h_o \times 2\pi r_o l} \\
 &= \frac{1}{5.8 \times 2\pi \times \frac{165}{1000} \times 1} \\
 &= 0.166
 \end{aligned}$$