

Q.1 assuming that a man can be represent by a cylinder of 30 cm in diameter and 1.7 m high with a surface temperature of 30 °C, calculate the heat he would be loss while standing in a 36 km/h wind at 10 °C. Use $Nu_D = 0.027 (Re_D)^{0.805} (Pr)^{1/3}$

And physical properties of air at 20 °C are $k=0.00259$ W/mk $Pr=0.707$, $\nu = 0.000015$ m²/s

Given Data

$$D = 30 \text{ cm} = 0.3 \text{ m}$$

$$L = 1.7 \text{ m}$$

$$T_s = 30^\circ\text{C}$$

$$T_{\infty} = 10^\circ\text{C}$$

$$T_{mf} = \frac{T_{\infty} + T_s}{2} = \frac{30 + 10}{2} = 20^\circ\text{C}$$

$$V = 36 \text{ km/h} = \frac{36 \times 1000}{3600} = 10 \text{ m/s}$$

$$k = 0.00259 \text{ W/mk}$$

$$Pr = 0.707$$

$$\nu = 0.000015 \text{ m}^2/\text{s}$$

$$Re = \frac{VD}{\nu} = \frac{10 \times 0.3}{0.000015}$$

$$Re = 200000$$

$$Pr = 0.707$$

$$Nu = 0.027 (Re)^{0.805} (Pr)^{1/3}$$

$$= 0.027 (200000)^{0.805} (0.707)^{1/3}$$

$$Nu = 770.24$$

$$Nu = \frac{hD}{k} \Rightarrow 770.24 = \frac{h \times 0.3}{0.00259}$$

$$h = 6.64$$

$$\Phi = h A_s (\tau_s - \tau_{\infty})$$

$$= 6.64 \times \pi \times D \times l (30 - 10)$$

$$= 6.64 \times \pi \times 0.3 \times 1.75 (30 - 10)$$

$$\boxed{\Phi = 213.08 \text{ W}}$$

Q.2 A motor cycle cylinder consists of fins having outside diameter 150 mm and total surface area of 0.27 m^2 . Calculate the rate of heat dissipation from cylinder fins when motorcycle is running at 20 m/s speed. The atmospheric air is at 25°C and average fin surface temperature is 475°C . The relevant thermo-physical properties at average temperature of 250°C are:

$$K = 0.0427 \text{ W/m}^\circ\text{C} \quad \nu = 40.61 \times 10^{-6} \text{ m}^2/\text{s} \quad \text{Pr} = 0.677$$

for turbulent flow use $\text{Nu} = 0.036 (\text{Re})^{0.8} (\text{Pr})^{0.33}$

Given Data

$$D = 150 \text{ mm} = 0.15 \text{ m}$$

$$A_s = 0.27 \text{ m}^2$$

$$V = 20 \text{ m/s}$$

$$T_{de} = 25^\circ\text{C}$$

$$T_s = 475^\circ\text{C}$$

$$T_{mf} = \frac{T_s + T_{de}}{2}$$

$$= \frac{475 + 25}{2}$$

$$= 250^\circ\text{C}$$

$$\text{Re} = \frac{VD}{\nu} = \frac{20 \times 0.15}{40.61 \times 10^{-6}} = 73873.43$$

$$\text{Pr} = 0.677$$

$$\begin{aligned} \text{Nu} &= 0.036 \times (\text{Re})^{0.8} \times (\text{Pr})^{0.33} \\ &= 0.036 \times (73873.43)^{0.8} \times (0.677)^{0.33} \\ &= 248.42 \end{aligned}$$

$$\text{Nu} = \frac{hD}{K}$$

$$248.42 = \frac{h \times 0.15}{0.0427}$$

$$h = 70.71 \text{ W/m}^2\text{K}$$

$$\Phi = h A_s (T_s - T_{de})$$

$$= 70.71 \times 0.27 \times (475 - 25)$$

$$= 8.591 \text{ kW}$$

Q.3 750 kg/hour of cream at 10°C is pumped through 1.75 m length of 8 cm inner diameter tube which is maintained at 95°C. estimate the temperature of cream leaving the heated section and the rate of heat transfer from the tube to the cream. The relevant thermo physical properties of cream are:

$$\rho = 1150 \text{ kg/m}^3$$

$$C_p = 2750 \text{ J/kg-deg}$$

Given Data

$$\dot{m} = 750 \text{ kg/hr} = \frac{7500}{3600} = 0.208 \text{ kg/s}$$

$$D = 8 \text{ cm} = 0.08 \text{ m}$$

$$L = 1.75 \text{ m}$$

$$\rho = 1150 \text{ kg/m}^3$$

$$C_p = 2750 \text{ J/kg}^\circ\text{C}$$

$$k = 0.42 \text{ W/m}^\circ\text{C}$$


$$T_i = 10^\circ\text{C}$$

$$T_s = 95^\circ\text{C}$$

$$\mu = 22.5 \text{ kg/ms}$$

$$k = 0.42 \text{ W/m-deg}$$

Use the following correlation for flow of cream inside a tube:

$$Nu = 3.65 + \frac{0.067 \left(\frac{D}{L} Re_{ed} Pr \right)}{1 + 0.04 \left(\frac{D}{L} Re_{ed} Pr \right)^{1/3}}$$


$$\dot{m} = \rho A V \quad A_c = \pi/4 d^2$$

$$0.208 = 1150 \times 5.026 \times 10^{-3} \times V \quad = \pi/4 \times 0.08^2 = 5.026 \times 10^{-3} \text{ m}^2$$

$$V = 0.0359 \text{ m/s}$$

$$Re = \frac{\rho V D}{\mu} = \frac{1150 \times 0.0359 \times 0.08}{22.5}$$

$$Re = 0.147$$

$$Pr = \frac{\rho C_p}{k} = \frac{22.5 \times 2750}{0.42} = 147321.42$$

using given Co-Relation

$$Nu = 3.65 +$$

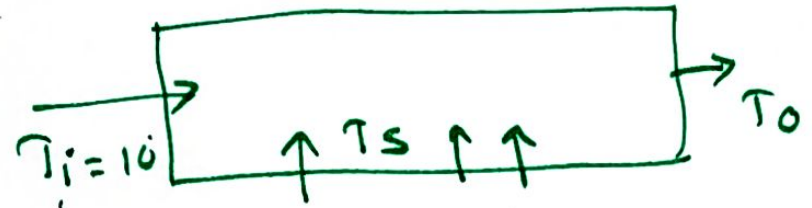
$$\frac{0.067 \left[\frac{0.08}{1.75} \times 0.147 \times 147321.42 \right]}{1 + 0.04 \left[\frac{0.08}{1.75} \times 0.147 \times 147321.42 \right]^{1/3}}$$

$$Nu = 51.45$$

$$Nu = \frac{hD}{k} \Rightarrow 51.45 = \frac{h \times 0.08}{0.42}$$

$$h = 270.11 \text{ W/m}^2\text{K}$$

$$\left. \begin{aligned} \phi &= hA \Delta T \\ \phi &= m c_p \Delta T \end{aligned} \right\}$$



$$hA \Delta T = m c_p \Delta T$$

$$270.11 \times \pi \times 0.08 \times 1.75 \times \left(95 - \left(\frac{T_o + 10}{2} \right) \right) = 0.208 \times 2750 \times (T_o - 10)$$

$$T_o = 25.99^\circ\text{C}$$

$$\phi = hA \Delta T$$

$$= 270.11 \times \pi \times 0.08 \times 1.75 \times (95 - 17.99)$$

$$\phi = 9147.73 \text{ W}$$